

U.S.N.

**B.M.S. College of Engineering, Bengaluru-560019**

Autonomous Institute Affiliated to VTU

**August 2024 Semester End Main Examinations****Programme: B.E.****Branch: Chemical Engineering****Course Code: 22CH4PCHTR****Course: Process Heat Transfer****Semester: IV****Duration: 3 hrs.****Max Marks: 100**

- Instructions:** 1. Answer any FIVE full questions, choosing one full question from each unit.  
 2. Missing data, if any, may be suitably assumed.  
 3. Use of steam tables is allowed.

<b>Important Note:</b> Completing your answers, compulsorily draw diagonal cross lines on the remaining blank pages. Revealing of identification, appeal to evaluator will be treated as malpractice.			<b>UNIT - I</b>	<b>CO</b>	<b>PO</b>	<b>Marks</b>
	1	a)	Derive an equation for steady state heat transfer through a composite wall, without heat generation and with constant thermal conductivity.	CO 2	PO 2	08
		b)	A furnace is constructed with thickness of 225 mm fire brick 120 mm of insulating brick and 225 mm of building brick. The inside temperature is 1200 K and outside temperature is 330 K. Find the heat loss per unit area and the temperature at the wall interface. Data: Thermal conductivity for fire brick is 1.4 W/mK Thermal conductivity for insulating brick is 0.2 W/mK Thermal conductivity for building brick is 0.7 W/mK	CO 3	PO 2	08
		c)	It is necessary to insulate a flat surface so that the rate of heat loss per unit area of the surface does not exceed 450 W/m <sup>2</sup> . The temperature difference across the insulating layer is 400 K. Evaluate the thickness of insulation if i. The insulation is made up of asbestos cement having thermal conductivity of. 0.11 W/mK. ii. The insulation is made up of fire clay having a thermal conductivity of 0.84 W/mK.	CO 3	PO 2	04
			<b>UNIT - II</b>			
	2	a)	Derive an expression for temperature profile and efficiency of an infinitely long rectangular fin.	CO 4	PO 2	12
		b)	One thousand spheres made of copper of diameter 3 mm are annealed in the annealing furnace. Initial temperature of the sphere is 20°C. Temperature of annealing furnace is 400°C. Given data: h = 30 kcal/m <sup>2</sup> h°C; C <sub>p</sub> = 0.8 kcal/kg °C. Compute the time required for the spheres to reach a temperature of 300°C.	CO 3	PO 2	08
			<b>OR</b>			

3	a)	Drive an equation for critical radius of insulation for spherical vessel insulated with a material of thermal conductivity K, state all assumptions	CO 4	PO 2	10
	b)	A steam pipe, 40 mm outside diameter is to be insulated by two layers of insulation, each 20 mm thick. The material A-1 has conductivity K, and material A-2 has conductivity 3 K. Assuming that the inner and outer surface temperatures of the composite insulation to be fixed, find which arrangement would give less heat loss rate, A-1 near pipe surface and A-2 as the outer layer or vice versa also calculate the percentage reduction in heat loss.	CO5	PO 3	10
		<b>UNIT - III</b>			
4	a)	Derive an expression for overall heat transfer coefficient by stating all assumptions. Define fouling and write expression for overall heat transfer coefficient including fouling.	CO5	PO 3	10
	b)	Illustrate briefly the following i. Pool boiling ii. Dropwise and film wise condensation	CO5	PO 3	10
		<b>OR</b>			
5	a)	Drive the expression of logarithmic mean temperature for counter flow heat exchanger, stating all the assumptions.	CO 5	PO 3	08
	b)	Derive Nusselt's equation for film wise condensation stating all the assumptions.	CO 5	PO3	12
		<b>UNIT - IV</b>			
6	a)	Illustrate the working of natural circulation evaporators with neat labelled diagrams.	CO 5	PO3	10
	b)	An evaporator is operating at atmospheric pressure. It is desired to concentrate feed from 5% solute to 20% solute by weight at a rate of 5000 kg/h. Dry saturated steam at a pressure corresponding to saturation temperature of 399 K is used. The feed is at 290 K and boiling point elevation is 5 K. Overall heat transfer coefficient is 2350 W/m <sup>2</sup> K. Compute the capacity, economy of evaporator and area of heat transfer to be provided. Data: Treating solution to be pure water and neglecting Boiling point. Latent heat of condensation of steam at 399 K is 2185 kJ/kg and latent heat of evaporation of water at atmospheric pressure and 373 K is 2257 kJ/kg. Specific heat of feed is 4.187 kJ/kgK.	CO 5	PO3	10
		<b>UNIT - V</b>			
7	a)	Briefly elaborate on i. Wien's displacement law ii. Plank's law iii. Kirchhoff's law of radiation	CO 1	PO1	10
	b)	Two large plane surface A and B situated at 2.5 mm apart in air. Surface A has an emissivity of 0.16 and it is at temperature of 400 K. Surface B has an emissivity of 0.08 and surface temperature is 350 K. Compute the heat transfer rate by radiation between two surfaces. Given: $\sigma = 5.62 \times 10^{-8} \text{ W/m}^2\text{K}^4$	CO 3	PO2	10