

B.M.S. College of Engineering, Bengaluru-560019

Autonomous Institute Affiliated to VTU

December 2023 Supplementary Examinations

Programme: B.E.

Branch: Chemical Engineering

Course Code: 22CH4PCMT1

Course: Mass Transfer-I

Semester: IV

Duration: 3 hrs.

Max Marks: 100

Instructions: 1. Answer any FIVE full questions, choosing one full question from each unit.
 2. Missing data, if any, may be suitably assumed.
 3. Use of steam table and humidity chart is allowed.

UNIT - I			CO	PO	Marks																
1	a)	List the various types of diffusions, based on the phases involved, number of components diffusing, and method of operation.	CO1	PO1	06																
	b)	Ammonia vapour is diffusing at a constant rate through a stagnant layer of air 1 mm thick. Conditions are fixed so that the gas contains 50% by volume of ammonia at one boundary of the stagnant layer. The ammonia diffusing to the other boundary is quickly absorbed and the concentration is negligible at that place. The temperature is 295 K and the pressure is atmospheric and under these conditions the diffusivity of ammonia in air is 0.18 cm ² /s. Calculate the rate of diffusion of ammonia through the layer. Data: partial pressure of ammonia is 0.5 atm.	CO3	PO2	06																
	c)	With a neat diagram, explain how diffusivity of acetone vapor is measured with the help of Arnold's diffusivity cell.	CO2	PO2	08																
OR																					
2	a)	Solute A is absorbed from a gas mixture of A and B with liquid flowing as a thin film downward along the wall of a tower. At a certain point in the tower, the bulk gas concentration is 0.38 mole fraction and the bulk liquid concentration is 0.1 mole fraction. Solute A is moving and B is stagnant in the gas phase and gets absorbed in a non-diffusing liquid. Use the equilibrium data and find the interface compositions in both the liquid and gas phases. Considering the solution to be dilute, estimate flux conditions. Data is given as follows.	CO3	PO2	10																
<table border="1" style="margin-left: auto; margin-right: auto;"> <tr> <td>x_A</td><td>0</td><td>0.05</td><td>0.10</td><td>0.15</td><td>0.20</td><td>0.25</td><td>0.30</td><td>0.35</td></tr> <tr> <td>y_A</td><td>0</td><td>0.022</td><td>0.052</td><td>0.087</td><td>0.131</td><td>0.181</td><td>0.265</td><td>0.385</td></tr> </table>			x_A	0	0.05	0.10	0.15	0.20	0.25	0.30	0.35	y_A	0	0.022	0.052	0.087	0.131	0.181	0.265	0.385	
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Important Note: Completing your answers, compulsorily draw diagonal cross lines on the remaining blank pages. Revealing of identification, appeal to evaluator will be treated as malpractice.

		$k_y = 1.465 \times 10^{-3} \text{ kmol/m}^2 \text{ s}$ mole fraction and $k_x = 1.967 \times 10^{-3} \text{ kmol/m}^2 \text{ s}$ mole fraction																					
	b)	Name the theories that explain the mechanism of mass transfer in turbulent flow. Explain any two of them with relevant sketches	CO2	PO2	10																		
		UNIT - II																					
3	a)	Draw the humidity chart with at least four psychometric properties and explain them.	CO1	PO1	10																		
	b)	A sample of air is at 1.013 bar and 35°C with a % saturation of 60%. It is required to alter the condition to i) temperature 25°C and humidity of 70% ii) Temperature 50 ° C and % humidity 30%. Recommend operations to achieve above stated conditions.	CO4	PO2	10																		
		OR																					
4	a)	Draw neat sketches of cooling tower arrangements and discuss	CO1	PO1	08																		
	b)	A forced draft cooling tower 5mx3m cross section is to cool 100 ton of water/h from 30°C to 13°C with air entering at 7.5°C and humidity of 0.004 kg water /kg dry air. Air leaves the tower at 19°C fully saturated. Estimate air velocity and makeup water required assuming a windage loss of 1% of water circulation rate. Saturation humidity of air at 19°C = 0.014 kg water / kg dry air. Latent heat of vaporization is 2460 kJ/ kg	CO3	PO2	12																		
		UNIT - III																					
5	a)	Draw the rate of drying curve showing the different zones of drying and explain the mechanism of drying in each zone.	CO1	PO1	10																		
	b)	1400 of bone dry granular solid is to be dried under constant drying conditions from moisture content of 0.2 kg/kg dry solid to a final moisture constant of 0.02 kg/kg dry solid. The material has an effective area of 0.0615 m ² /kg dry solid. Under the same conditions the following rate were previously known. Calculate the time required for drying.	CO3	PO2	10																		
		<table border="1"> <thead> <tr> <th>X, kg moisture/kg dry solid</th> <th>Rate of drying, N, kg/h/m²</th> </tr> </thead> <tbody> <tr><td>0.3</td><td>1.71</td></tr> <tr><td>0.2</td><td>1.71</td></tr> <tr><td>0.14</td><td>1.71</td></tr> <tr><td>0.096</td><td>1.46</td></tr> <tr><td>0.056</td><td>1.29</td></tr> <tr><td>0.046</td><td>0.88</td></tr> <tr><td>0.026</td><td>0.54</td></tr> <tr><td>0.016</td><td>0.376</td></tr> </tbody> </table>	X, kg moisture/kg dry solid	Rate of drying, N, kg/h/m ²	0.3	1.71	0.2	1.71	0.14	1.71	0.096	1.46	0.056	1.29	0.046	0.88	0.026	0.54	0.016	0.376			
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6	a)	Compare physical adsorption with chemisorption	CO1	PO1	04																		

	b)	Give the list of any three adsorbents commonly used. Mention their applications.	CO1	PO1	04																				
	c)	Air is being dried by passing it over silica gel. In a particular operation, 600 cm^3 of moist air measured at 25°C and 1 atm. pressure with an initial moisture content equivalent to 22 mm Hg pressure is passed over certain weight of silica gel (with an initial residual moisture content of 5 g. of moisture per 100 g of dry gel) until the gel has attained 15 g of moisture per 100 g of dry gel. The resulting air is passed over new silica gel of equal quantity as used in the first operation. Calculate i) the least moisture content of air that can be obtained ii) the final moisture content of silica gel Equilibrium data:	CO3	PO2	12																				
		<table border="1"> <tr> <td>g moisture/ 100 gm Gel</td> <td>0</td> <td>5</td> <td>10</td> <td>15</td> <td>20</td> <td>25</td> <td>30</td> <td>35</td> <td>40</td> </tr> <tr> <td>Partial pressure of water, mm Hg</td> <td>0</td> <td>2.1</td> <td>4.7</td> <td>7.1</td> <td>9.1</td> <td>10</td> <td>13</td> <td>14</td> <td>16.7</td> </tr> </table>				g moisture/ 100 gm Gel	0	5	10	15	20	25	30	35	40	Partial pressure of water, mm Hg	0	2.1	4.7	7.1	9.1	10	13	14	16.7
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7	a)	Discuss the methods of saturation and super saturation of a solution before crystallization giving suitable examples.	CO1	PO1	06																				
	b)	What is caking in crystallization? How is it prevented?	CO1	PO1	04																				
	c)	A Swenson Walker crystallizer is used to crystallize $\text{Na}_2\text{SO}_4 \cdot 10\text{H}_2\text{O}$ at the rate of 1000 kg/h. by cooling a saturated solution of Na_2SO_4 from 40°C to 17°C . Cooling water enters the unit at 12°C and leaving at 27°C . Evaporation is negligible. The solubility of anhydrous Na_2SO_4 in water are 49 and 15 kg/100 kg water at 40°C and 17°C , respectively. Calculate the feed and mother liquor flow rates.	CO3	PO2	10																				
