

# B.M.S. College of Engineering, Bengaluru-560019

Autonomous Institute Affiliated to VTU

## October 2024 Supplementary Examinations

Programme: B.E.

Branch: Chemical Engineering

Course Code: 23CH4PCTD2

Course: Process Engineering Thermodynamics-II

Semester: IV

Duration: 3 hrs.

Max Marks: 100

**Instructions:** 1. Answer any FIVE full questions, choosing one full question from each unit.  
2. Missing data, if any, may be suitably assumed.

Important Note: Completing your answers, compulsorily draw diagonal cross lines on the remaining blank pages. Revealing of identification, appeal to evaluator will be treated as malpractice.			<b>UNIT - I</b>	<b>CO</b>	<b>PO</b>	<b>Marks</b>
	1	a)	Show that, $dU = [CP - PV\alpha] dT + V[P\beta - T\alpha] dP$ <p>Where, <math>\alpha</math> = Co efficient of expansion; and <math>\beta</math>= Coefficient of compression.</p>	CO1	PO1	12
		b)	Mercury has a density of 13690 kg/m <sup>3</sup> in the liquid state and 14193 kg/m <sup>3</sup> in the solid state, both measured at the melting point of 234.33 K at 1 bar. Estimate the melting point of mercury at a pressure of 10 bar. The heat of fusion of mercury around 9.7876 kJ/kg.	CO2	PO2	08
			<b>OR</b>			
	2	a)	At 573 K and pressures of 0–6.0 MPa, the Joule-Thomson coefficient of N <sub>2</sub> (g) can be represented as $\mu = 0.14 - 2.533 \times 10^{-2} P$ <p>Where, <math>\mu</math> is in <math>\left(\frac{K}{MPa}\right)</math>. Assuming this equation to be temperature-independent near 573 K, find the temperature drop which may be expected in the Joule-Thomson expansion of the gas from 6.0 MPa to 2.0 MPa pressure.</p>	CO 3	PO2	10
		b)	Derive Gibbs Helmholtz equation with suitable assumptions.	CO3	PO2	10
			<b>UNIT - II</b>			
	3	a)	Determine fugacity coefficient from compressibility factor.	CO3	PO2	08
		b)	Deduce Gibbs -Duhem equation from the fundamental partial molar properties. Mention various forms of Gibbs -Duhem equation.	CO3	PO2	12
			<b>OR</b>			
	4	a)	Explain the tangent intercept method for the estimation of partial molar property.	CO3	PO2	10

	b)	Calculate the partial molar volume of water in a 50 mole % ethanol-water solution in which the partial molar volume of ethanol is $52.37 \times 10^{-6} \text{ m}^3/\text{mol}$ . Data: The density of solution is $800.21 \text{ kg/m}^3$ .	CO3	PO2	10
		<b>UNIT - III</b>			
5	a)	Derive the criteria for phase equilibrium for the following conditions i. Constant U and V ii. Constant T and V iii. Constant P and T	CO4	PO3	12
	b)	A binary liquid mixture consists of 60 mol percent ethylene and 40ml percent propylene. At 423 K, the vapour pressure of ethylene and propylene are 15.2 atm and 9.8 atm respectively. Calculate the total pressure and equilibrium composition of the vapour phase. Assume that the mixture behaves like an ideal gas.	CO4	PO3	08
		<b>UNIT - IV</b>			
6	a)	Sketch and explain minimum boiling and maximum boiling azeotrope.	CO5	PO3	12
	b)	An equimolar solution of benzene and toluene is totally evaporated at constant temperature of 363 K. At this temperature, the vapor pressure of benzene and toluene are 135.4 and 54 kPa, respectively. Calculate the pressures at the beginning and at the end of the vaporization.	CO5	PO3	08
		<b>UNIT - V</b>			
7	a)	Discuss reaction coordinate and establish the equation for mole fraction of component 'i', in the reaction mixture is given by $y_i = \frac{n_i}{n} = \frac{n_{i0} + \gamma_1 \varepsilon}{n_0 + \gamma \varepsilon}$	CO6	PO3	12
	b)	The following reaction takes place in a system consisting of 3 mol $\text{CH}_4$ , 1 mol $\text{H}_2\text{O}$ , 1 mol $\text{CO}$ and 4 mol $\text{H}_2$ initially: $\text{CH}_4 + \text{H}_2\text{O} \rightarrow \text{CO} + 3\text{H}_2$ Express the composition of the mixture in terms of mole fraction as a function of extent of reaction.	CO6	PO3	08

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