

U.S.N.

B.M.S. College of Engineering, Bengaluru-560019

Autonomous Institute Affiliated to VTU

January / February 2025 Semester End Main Examinations

Programme: B.E.

Semester: V

Branch: Chemical Engineering

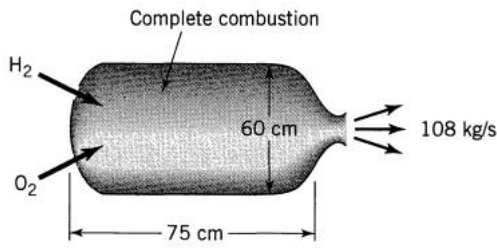
Duration: 3 hrs.

Course Code: 23CH5PCCR1 / 22CH5PCCR1

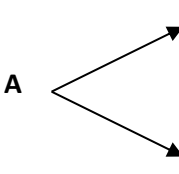
Max Marks: 100

Course: Chemical Reaction Engineering I

Instructions: 1. Answer any FIVE full questions, choosing one full question from each unit.
2. Missing data, if any, may be suitably assumed.

Important Note: Completing your answers, compulsorily draw diagonal cross lines on the remaining blank pages. Revealing of identification, appeal to evaluator will be treated as malpractice.			UNIT - I	CO	PO	Marks
	1	a)	Define reaction rate based on various units and list the factors affecting the rate of reaction.	CO1	PO2	07
		b)	Discuss the salient features of collision and transition state theories.	CO1	PO2	06
		c)	Milk is pasteurized if heated to 63 °C for 30 min, but it only needs 15 s to achieve the same result if heated to 74°C. Find the activation energy of this sterilization process.	CO1	PO2	07
			OR			
	2	a)	Discuss molecularity and order of reaction with suitable examples.	CO1	PO2	04
		b)	Discuss how different variables affect the rate of reaction with suitable examples.	CO1	PO2	06
		c)	A rocket engine burns a stoichiometric fuel mixture (liquid hydrogen) and an oxidant (liquid oxygen). The combustion chamber is cylindrical, 75 cm long, and 60 cm in diameter, and the combustion process produces 108 kg/s of exhaust gases. If combustion is complete, find the hydrogen and oxygen reaction rate.	CO1	PO2	10
						
			UNIT - II			
	3	a)	Define an elementary and non-elementary reaction and explain the kinetic models for non-elementary reactions.	CO2	PO2	10
		b)	Experiments show that the reaction between $H_2(g)$ and $I_2(g)$ to produce $HI(g)$ proceeds with a rate	CO2	PO2	10

		$\frac{1}{2} \frac{d[HI]}{dt} = k [H_2][I_2]$ <p>Suggest a two-step mechanism that is consistent with this rate.</p>																							
		OR																							
4	a)	The reaction between CO and NO ₂ at low temperatures proceeds with the rate: $-r_{NO_2} = k[NO_2]^2$ <p>Suggest a mechanism to explain this rate.</p>	CO2	PO2	10																				
	b)	Mention the different methods used to analyze the kinetic data. Explain any one method with help of graphical interpretation.	CO2	PO2	10																				
		UNIT - III																							
5	a)	Develop a design equation of a stirred tank reactor for a constant density system.	CO3	PO3	10																				
	b)	The following kinetic data are obtained in a constant volume batch reactor at 273 K using pure gaseous A, and the partial pressure of A is given in mm Hg. <table border="1"><tr><td>Time, min</td><td>0</td><td>2</td><td>4</td><td>6</td><td>8</td><td>10</td><td>12</td><td>14</td><td>∞</td></tr><tr><td>Partial pressure</td><td>760</td><td>600</td><td>475</td><td>390</td><td>320</td><td>275</td><td>240</td><td>215</td><td>150</td></tr></table>	Time, min	0	2	4	6	8	10	12	14	∞	Partial pressure	760	600	475	390	320	275	240	215	150	CO3	PO3	10
Time, min	0	2	4	6	8	10	12	14	∞																
Partial pressure	760	600	475	390	320	275	240	215	150																
		OR																							
6	a)	From the following data, find a satisfactory rate equation for the gas phase decomposition A → R + S occurring isothermally in a mixed-flow reactor. <table border="1"><tr><td>Run Number</td><td>1</td><td>2</td><td>3</td><td>4</td><td>5</td></tr><tr><td>τ, s</td><td>0.423</td><td>5.10</td><td>13.5</td><td>44</td><td>192</td></tr><tr><td>X_A</td><td>0.22</td><td>0.63</td><td>0.75</td><td>0.88</td><td>0.96</td></tr></table> <p>All the runs are conducted with $C_{A0} = \frac{0.002 \text{ mol}}{l}$, i.e., with the same initial concentration.</p>	Run Number	1	2	3	4	5	τ, s	0.423	5.10	13.5	44	192	X _A	0.22	0.63	0.75	0.88	0.96	CO3	PO3	14		
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τ, s	0.423	5.10	13.5	44	192																				
X _A	0.22	0.63	0.75	0.88	0.96																				
	b)	The half-life for converting ammonium cyanate into urea at 303 K at initial concentrations of ammonium cyanate of 0.1 mol/l and 0.2 mol/l is 1152 min and 568 min, respectively. Determine the order of the reaction.	CO3	PO3	06																				
		UNIT - IV																							
7	a)	What are the guidelines for the best arrangement of a combination of reactors?	CO4	PO3	08																				
	b)	A gas mixture containing 50 mole % A and 50 mole % inerts at 10 atm enters a reactor system with a flow rate of 6 L/s at 144 °C. The laboratory measurements of the rate as a function of conversion at 144°C and 10 atm are:	CO4	PO3	12																				

			<table><tr><td>X_A</td><td>0</td><td>0.1</td><td>0.2</td><td>0.3</td><td>0.4</td><td>0.5</td><td>0.6</td><td>0.7</td><td>0.8</td><td>0.85</td></tr><tr><td>$-r_A \times 10^{-2}$</td><td>0.53</td><td>0.52</td><td>0.5</td><td>0.45</td><td>0.4</td><td>0.33</td><td>0.25</td><td>0.18</td><td>0.125</td><td>0.1</td></tr></table> <p>If the reaction is carried out in two reactors in series, with 40% conversion in the first reactor and 85 % overall conversion. Estimate the total volume of the two reactors when</p> <p>i. Mixed flow reactor is used. ii. Plug flows reactor is used.</p>	X_A	0	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.85	$-r_A \times 10^{-2}$	0.53	0.52	0.5	0.45	0.4	0.33	0.25	0.18	0.125	0.1			
X_A	0	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.85																		
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			OR																									
	8	a)	Explain the graphical method to find the conversion in a series of mixed-flow reactors of different sizes.	CO4	PO3	8																						
		b)	Liquid reactant A produces R and S by the following reactions in parallel. $A \rightarrow R \quad r_R = 0.40 C_A^2 \quad k_1 = 0.4 m^3 / (mol. min)$ $A \rightarrow S \quad r_S = 0.40 C_A \quad k_2 = 0.2 (min)^{-1}$ A feed of aqueous A with $C_{Ao} = 40 mol/m^3$ enters a reactor, reacts to produce R and S, and a mixture of A, R and S leaves the reactor. Find C_S, C_R and τ for 90 % conversion of A in a mixed flow reactor.	CO4	PO3	12																						
			UNIT - V																									
	9	a)	What is optimum temperature progression? Discuss the optimum temperature progression for irreversible, reversible endothermic, reversible exothermic reactions.	CO5	PO2	12																						
		b)	For the competitive liquid-phase reaction: $\frac{dC_R}{dt} = C_A C_B^{0.3} \text{ mol/l min}$ <div style="display: flex; align-items: center; justify-content: center;"><div style="text-align: center;"><p>A</p></div><div style="margin-left: 20px;">$\frac{dC_R}{dt} = C_A C_B^{0.3} \text{ mol/l min}$ $\frac{dC_S}{dt} = C_A^{0.5} C_B^{1.8} \text{ mol/l min}$</div></div> <p>Find the fraction of impurities in the product stream for 90% conversion of pure A and pure B, each having a concentration of 20 mol/L for (a) PFR and (b) MFR</p>	CO5	PO2	08																						
			OR																									
	10	a)	What are the instantaneous fractional yield, overall fractional yield, and selectivity in the case of parallel reaction schemes? Explain with equations.	CO5	PO2	08																						
		b)	Explicate the general graphical design procedure for a single homogeneous non-isothermal reaction.	CO5	PO2	12																						
